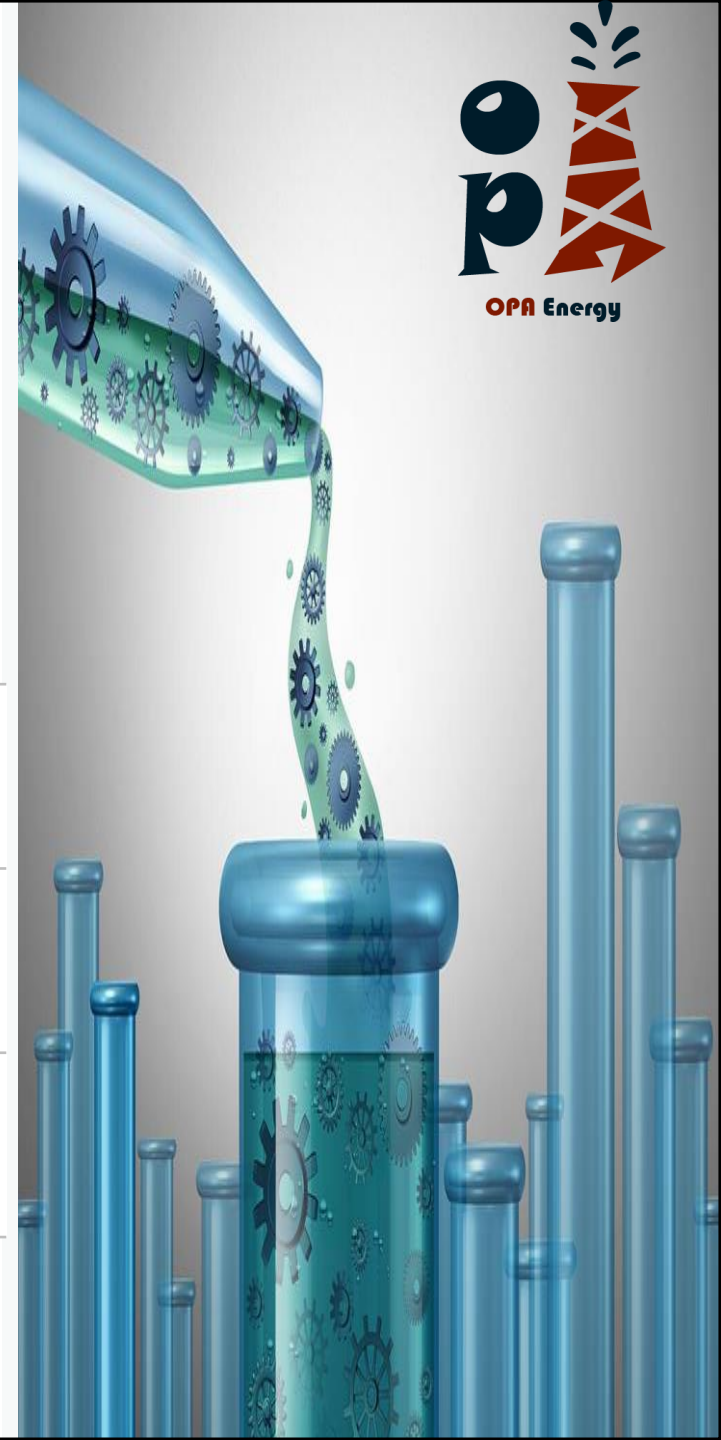


Understanding Reservoir Fluids & PVT Modeling

- Reservoir Fluid Behavior
- Why Predict Fluid Behavior ?
- Types of Fluid Models
- EOS Modeling: A Brief Review



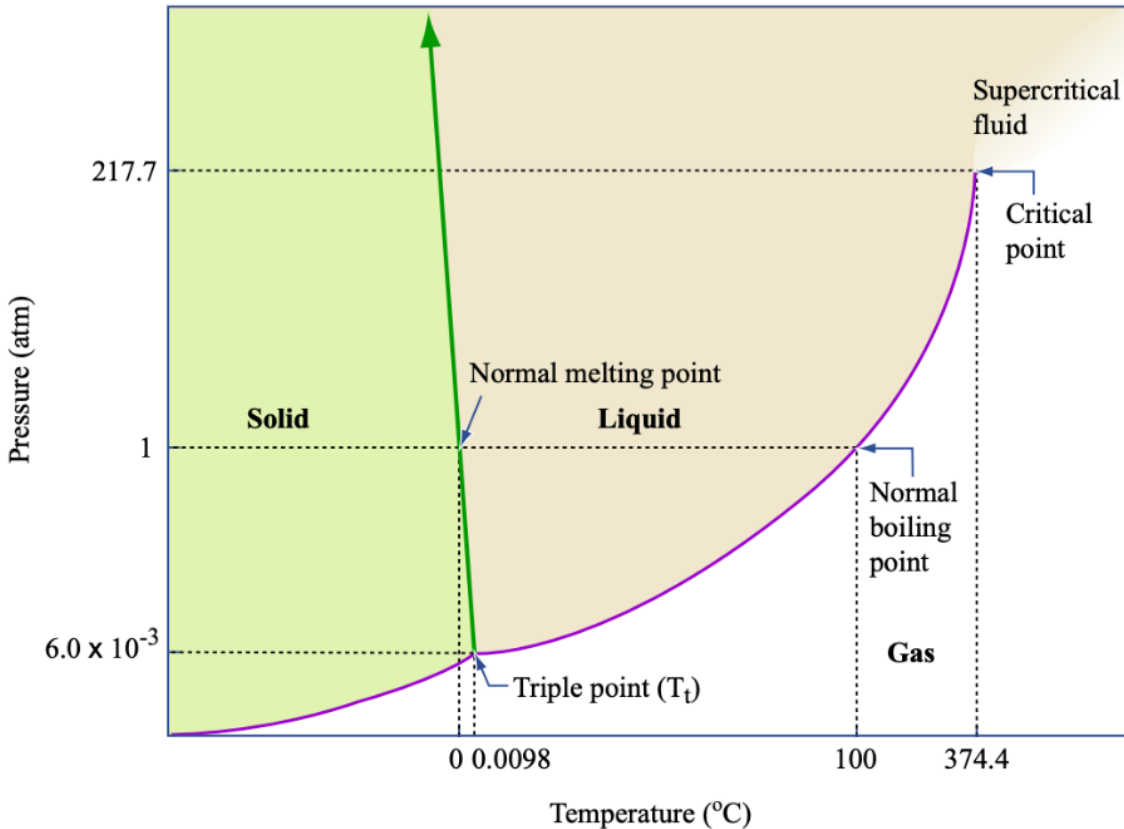
◎ Reservoir Fluids: Types & Behavior

- Reservoir fluids are generally complex mixtures of hydrocarbons existing as “liquid-gas” systems under high pressures & temperatures.
- Seldom are two crude oil samples identical and seldom are two crude oils made up of the same proportions of the various compounds.

Fluid Types

- Dry Gases
- Wet Gases
- Gas Condensate
- Volatile Oils
- Black Oils

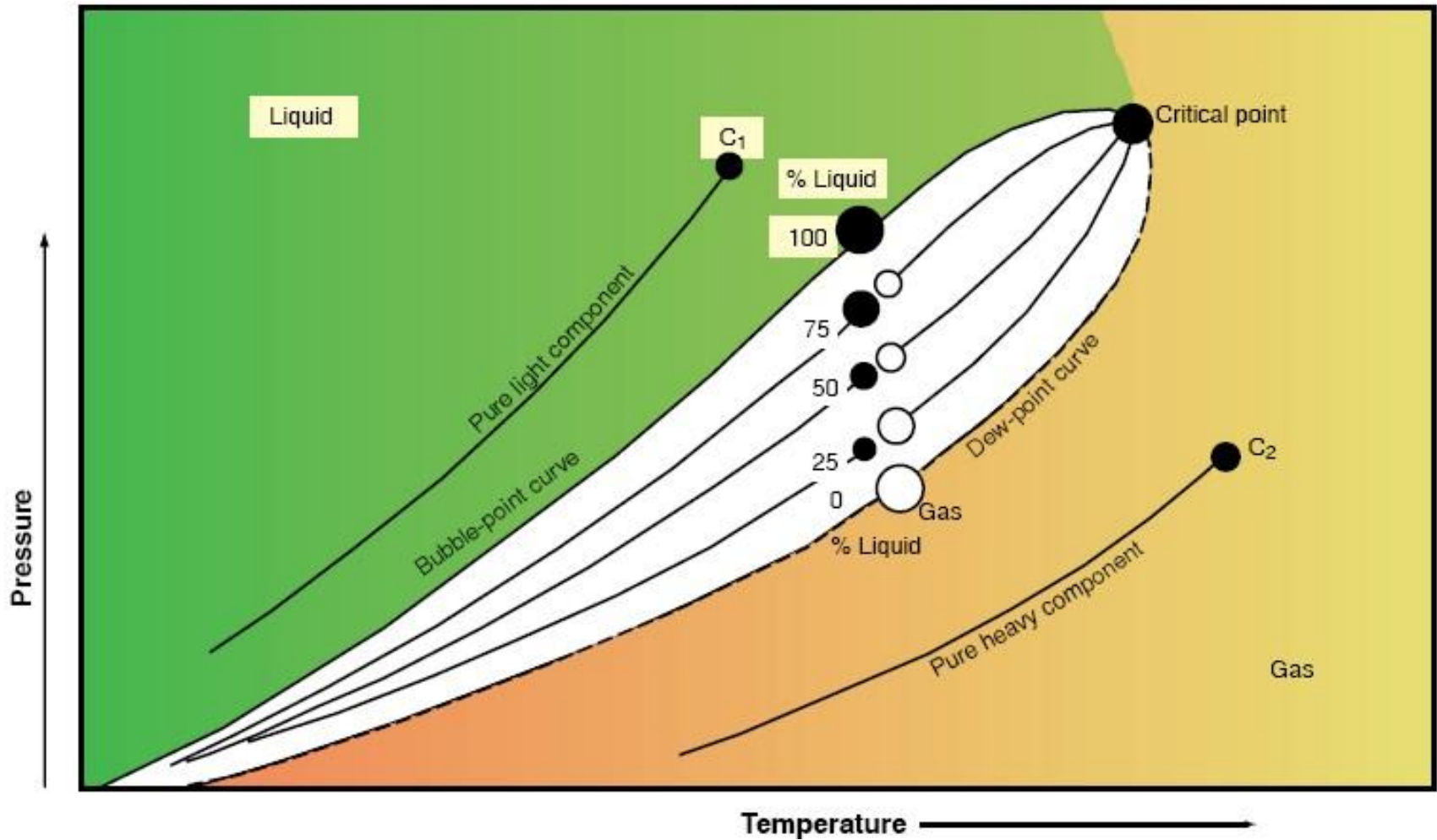
Phase Diagram Pure Substance (P-T)



- For a single component system, phase behavior is primarily defined by two lines: vapor pressure curve and melting point curve
- Critical point: represents the conditions above which liquid and gas phases cannot be distinguished
- Triple point: condition at which all three phases can exist under equilibrium conditions

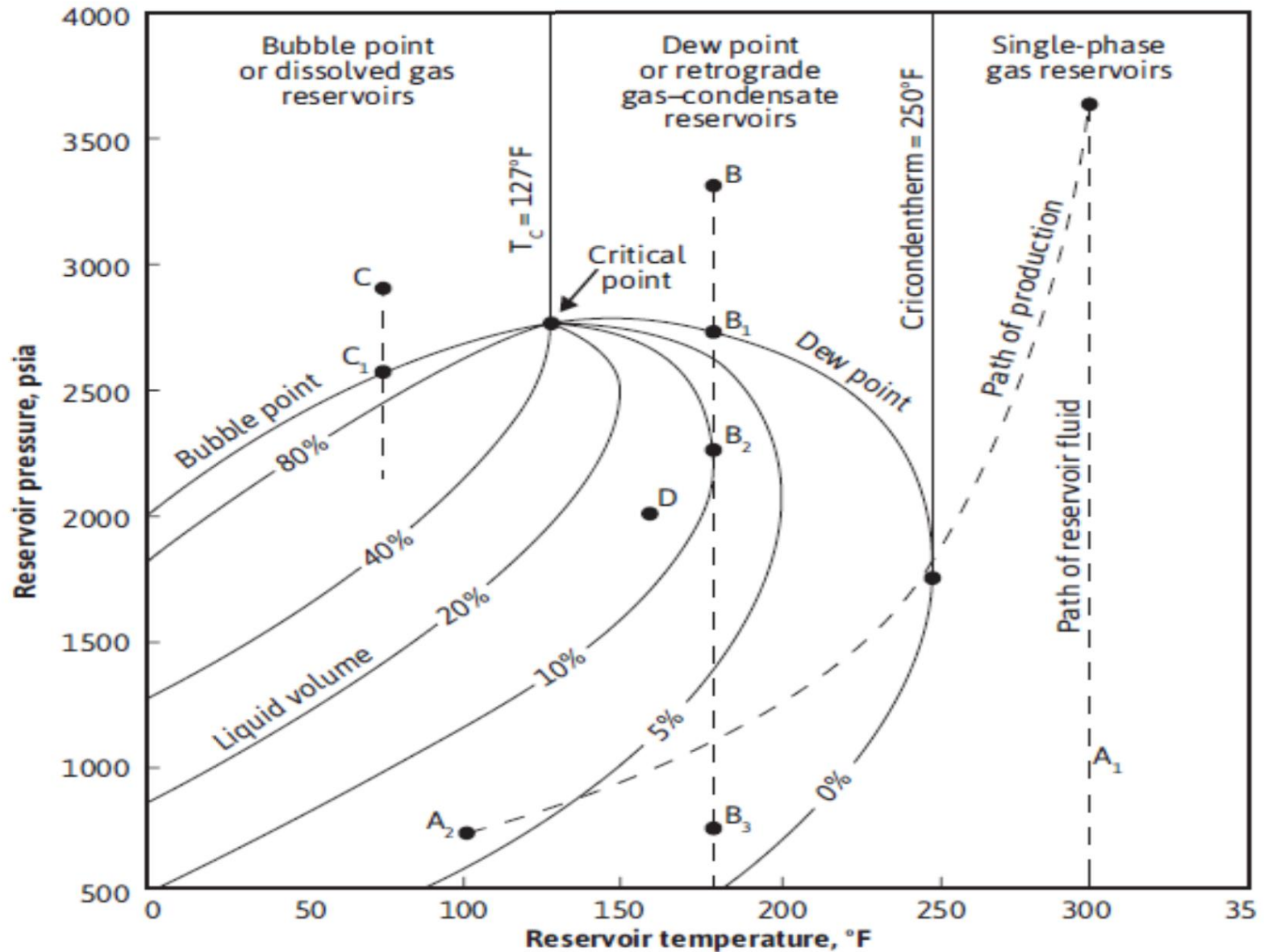
Phase Diagram of Water

Phase Behavior of a Multi-Component System



50:50 mixture of two pure hydrocarbon components on the P-T plane

Phase Diagram – Mixture



◎ Why Predict Fluid Behavior ?

- In oil and gas production systems, all models—whether reservoir, well, surface network, or processing facility, have at least one common input between them –

“How the fluid properties change with pressure and temperature as it travels from location A to B”

- As this is a basic input, it is imperative we have a good understanding/description of how the fluid behaves at different conditions.

Fluid Models



BO Correlations

- Relates fluid properties at surface (API, GOR, Gas gravity) to properties at downhole (B_o , P_b , R_s , etc.)

Pros:

- Fast and accurate

Cons:

- Not Valid outside their Experimental ranges
- No output composition



Equation of State

- Thermodynamic equations that predict the behavior of fluids based on their composition

Pros:

- Get composition of fluid at any P and T

Cons:

- Slow in calculations
- Weak for density calculations
- Does not respect Mass balance

● Workflow Summary in PVT Program

QC Lab Data

- Composition
- Mass Balance
- Experiments Consistency

Define Pure Components

- Select Components
- Enter Composition

Define Pseudo Components

- Mw, SG & BPT
- Pseudo Splitting
- BICs

Enter Lab Data

- Select Data for Regression
- Select Weighting

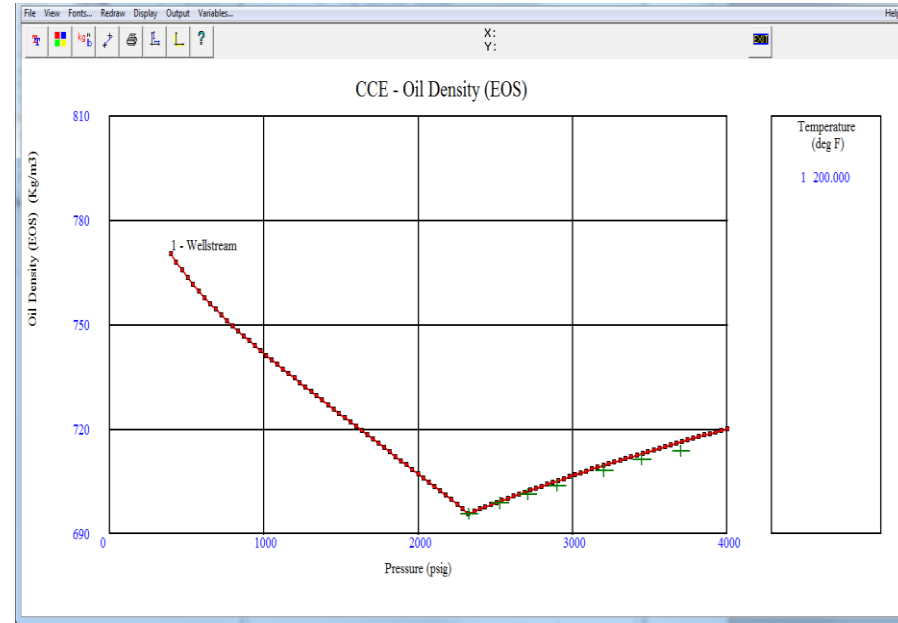
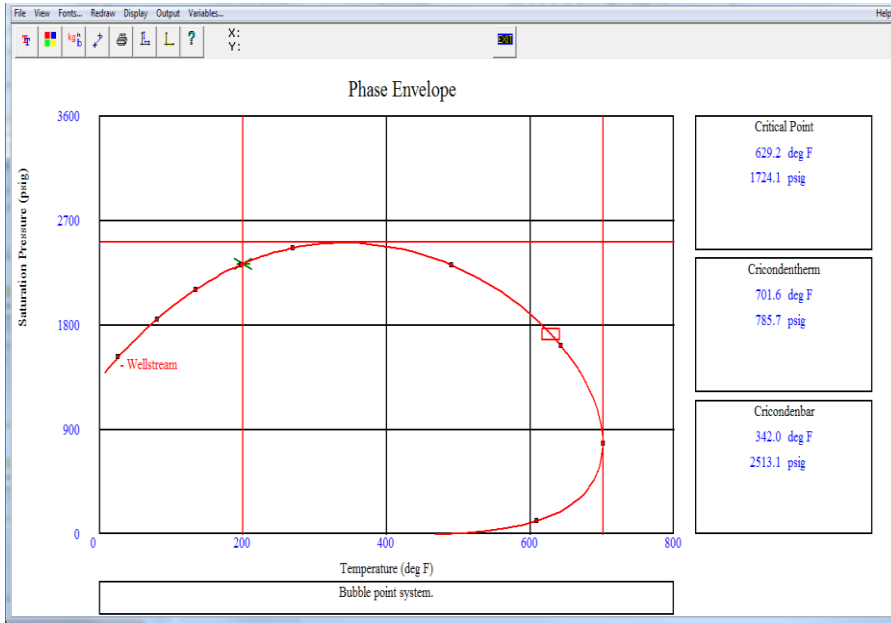
Regression

- Develop Regression Strategy
- Regress
- Quality Check

EOS Validation

- Reproduce Lab Experiments

Q/C the EOS Model – Phase Envelope/CCE/SEP prediction



Oil Reservoir Ex.1 - Calculation Results

Temperature (deg F)	Pressure (psig)	Gas Density (EOS) (Kg/m3)	Oil Density (EOS) (Kg/m3)	Oil Dens. (COSTALD) (Kg/m3)	Interfacial Tension (dyne/cm)	Gas Viscosity (centipoise)
70	400	25.0397	794.531	792.084	18.3775	0.0114573
60	0	1.5102	828.9	816.674	24.0043	0.00937293

Wellstream

Oil Reservoir Ex.1 - Calculation Results

Temperature (deg F)	Pressure (psig)	Gas FVF (ft3/scf)	Oil FVF (RB/STB)	Gas Oil Ratio (scf/STB)	Specific Enthalpy (Vap) (BTU/lbmol)	Specific Enthalpy (Liq) (BTU/lbmol)
70	400	0.0325652	1.11515	423	8787.65	21385.9
60	0	1	1	214.7	12526	25585.5

Wellstream